



Viscosity evaluation of ZrO_2 dispersed molten stainless



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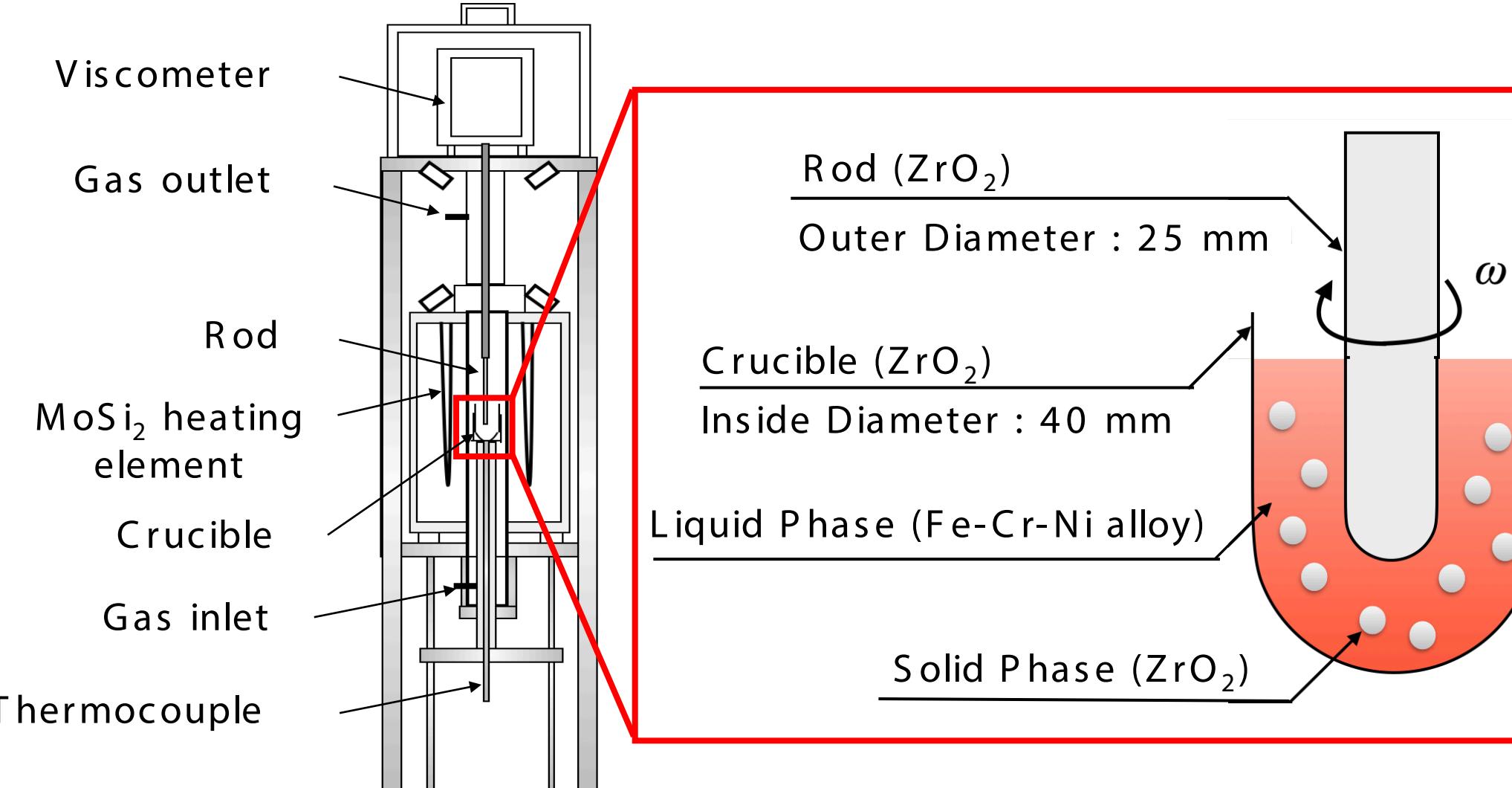
Introduction

The flow behavior of high-temperature suspensions is industrially crucial, such as in the steelmaking process¹⁾

However, due to the experimental challenges, there is limited understanding of high-temperature suspensions.

To address this, samples with a minimal density difference between the solid and liquid phases were selected, aiming to study the detail of the flow behavior of high-temperature suspensions.

Experimental

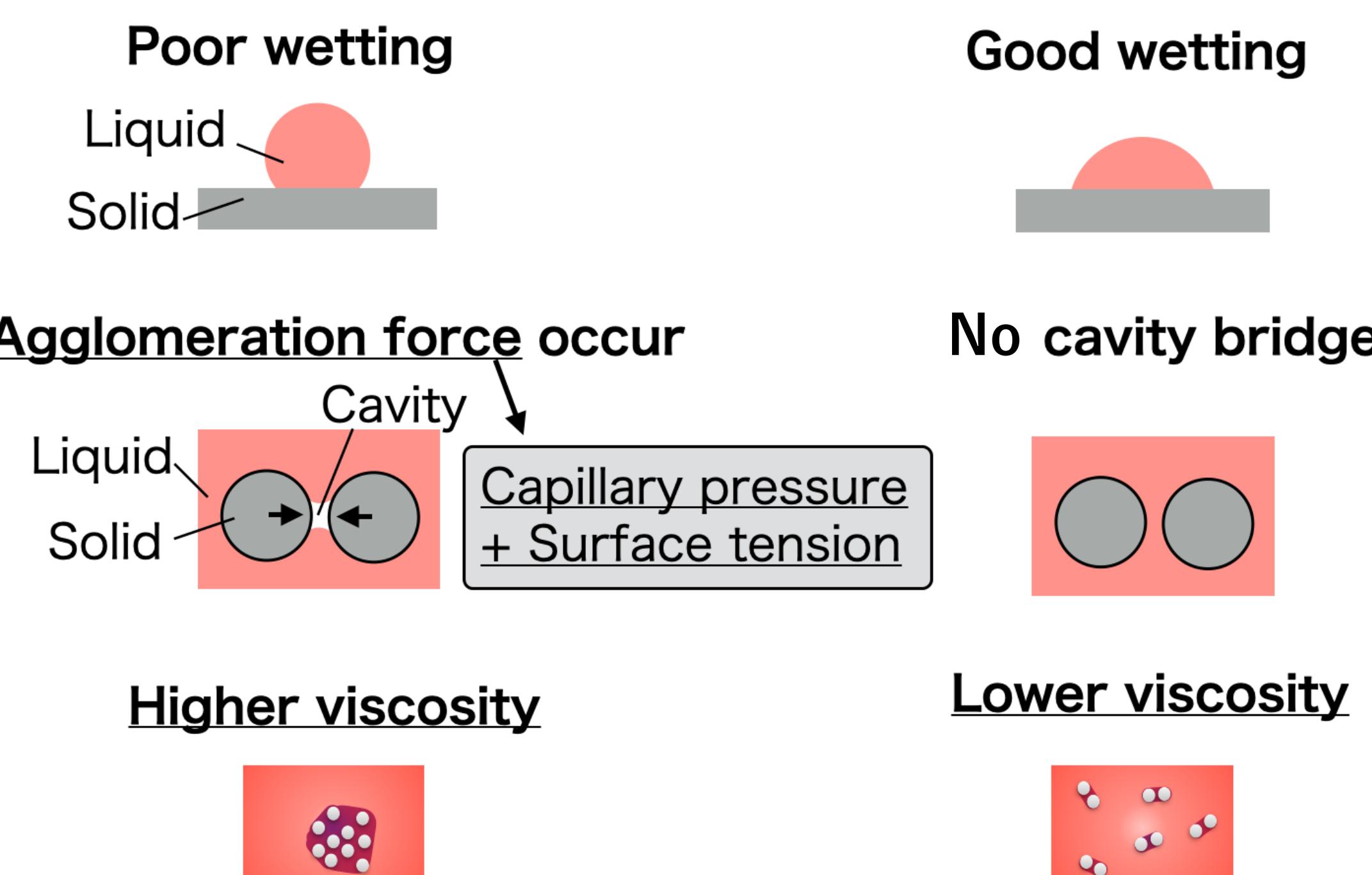


Viscosity measuring device with concentric cylinder method

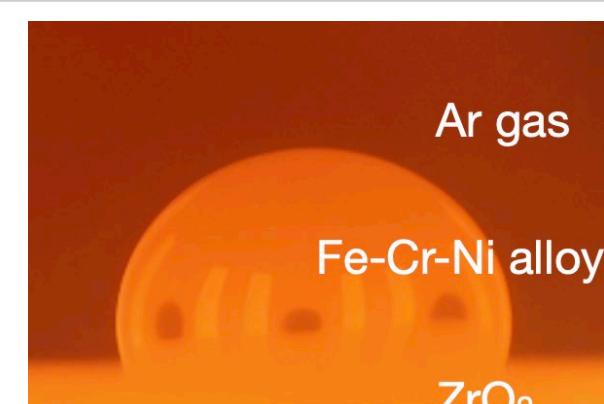
Measuring conditions

Sample	ZrO_2 beads dispersed in molten Fe-Cr-Ni alloy
Solid phase (ZrO_2 beads)	5 vol% to 60 vol%
Shear Rates	67 s^{-1} to 202 s^{-1}
Temperature	1773 K
Gas Flow	Ar-5%H ₂ (2 L/min)

Dependence of suspension viscosity on solid-liquid interfacial property^{5,6)}



The volume of the immobilized fluid increases due to the agglomeration, leading to an increase in viscosity.



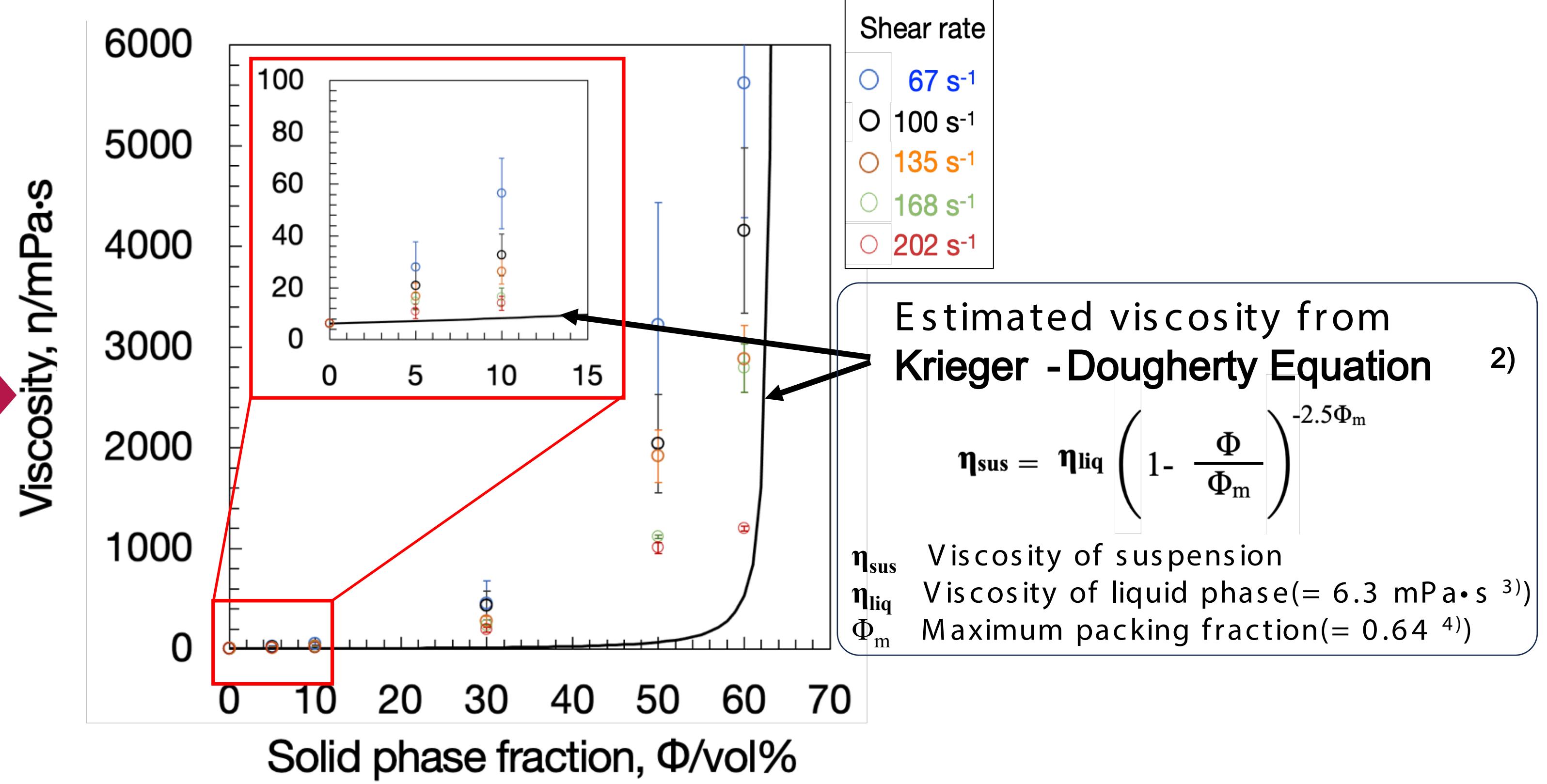
The contact angle between molten alloy and ZrO_2 was 108.8° (Poor wetting) at 1773 K in an Ar atmosphere.

Conclusion

- The measured viscosity increased with an increase in solid phase fraction.
- The findings indicate that the measured viscosity was higher than predicted by the KD equation.
- It is hypothesized that these cohesive forces lead to agglomeration, which contribute to the increased viscosity.
- The potential influence of interfacial properties between solid and liquid phases on the viscosity of suspensions has been suggested. Further research is required to consider maximum packing fraction (Φ_m) to get better estimation of the suspension viscosity.

Results and Discussions

Viscosity dependence on the solid phase in ZrO_2 dispersed molten Fe-Cr-Ni alloy



Viscosity increased with an increase in solid phase fraction
Measured viscosity > Estimated viscosity by KD equation
The KD equation neglects interactions between solid phases

The significant deviation from estimations is due to the lack of consideration for solid-liquid interfacial properties.

Estimating viscosity with agglomeration force

The agglomeration force F between the solid phases is⁷⁾

$$F = 2\pi \frac{R_1 R_2}{R_1 + R_2} 2\sigma_{LG} \cos\theta = 870 \mu\text{N}$$

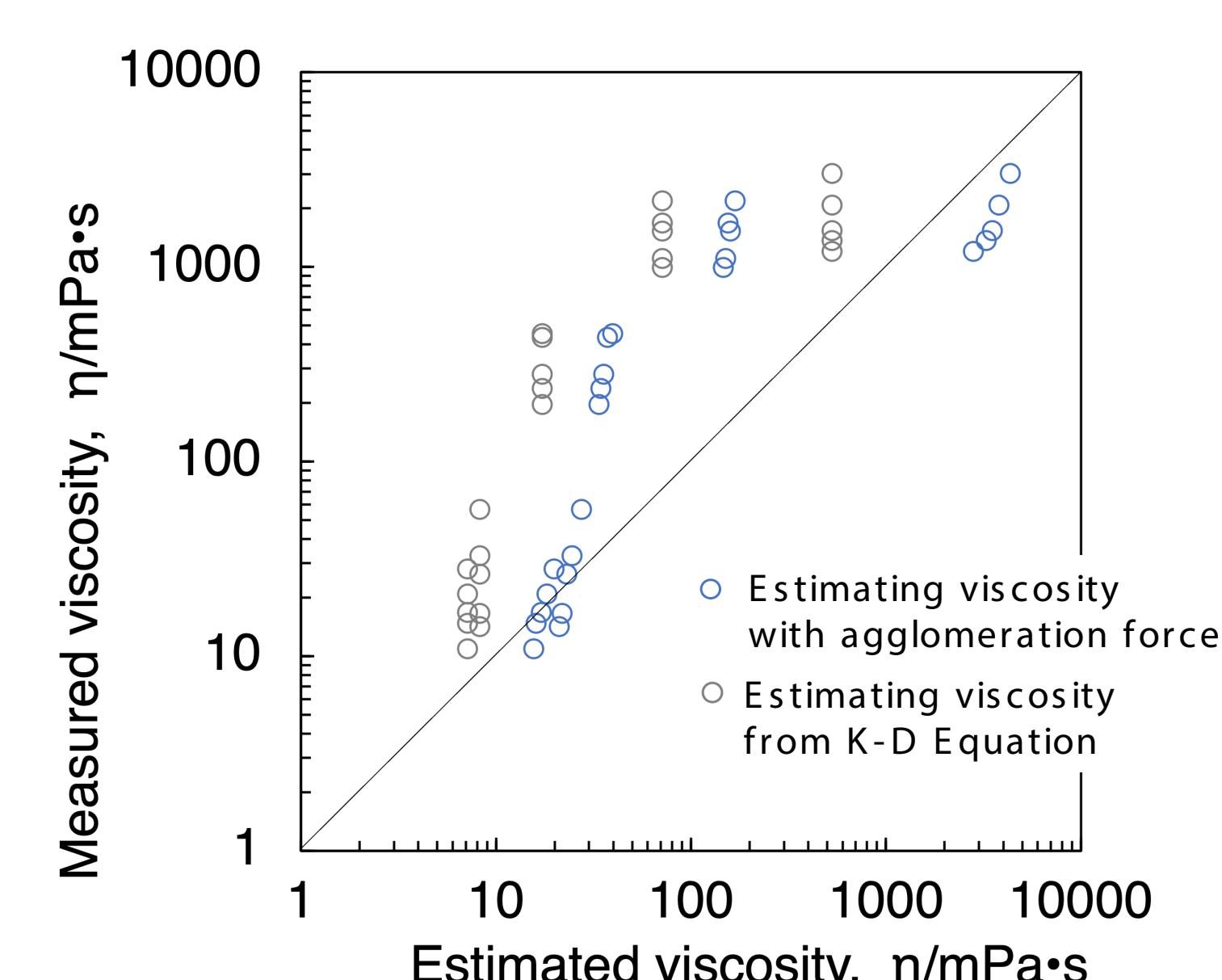
R_1, R_2 : Radius of dispersed solid ($= 250 \mu\text{m}$)
 σ_{LG} : Surface tension of liquid phase ($= 1.721 \text{ N/m}^4$)
 θ : Contact angle 108.8°

The agglomeration force F between the solid phases is much larger than Van der Waals force ($10^{-5} \mu\text{N}^5$) and buoyancy force ($0.51 \mu\text{N}^5$).

The apparent solid fraction during cluster formation is⁶⁾

$$\Phi_{\text{eff}} \approx \Phi \left(1 + \left(\frac{F}{\gamma \eta_{\text{sus}}} \right)^{1/3} \right)^{3-f}$$

γ : Shear rate
 η_{sus} : Viscosity of suspension
 f : Fractal dimension ($1 < f < 3$)



Considering the agglomeration force leads to a better